# Reducing the Effect of Torque on SISO Gas Turbine System by Applying Suitable $H_{\infty}$ Controller

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**Abstract**— This paper describes the robust control of single input-single output (SISO) gas turbine system by employing suitable  $H_{\infty}$ Controller. A non-linear model of this system has been taken from literature and developed to a linear model, the state space  $H_{\infty}$  controller is performed using this linearized model. The performance criteria are specified in terms of bandwidth and desired response of the system. The employed  $H_{\infty}$  is compared to a classical Proportional-Integral Drifted (PID) controller, the results show that the  $H_{\infty}$  Controller is best.

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Index Terms—  $H_{\infty}$  Controller, Modeling of SISO gas turbine, Robust control, Simulation by MATLAB.

### **1** INTRODUCTION

The gas turbines are important and widely employed in transportation and power systems [1]. For developing a control strategy of a gas turbine system there are diverse stages such as; specifying the performance requirements, modeling of the system, designing the controller and validating the controller design by simulating the nonlinear closed loop system [2]. The ability of the closed loop system in responding to a sudden change in the speed is the term of specifying the desired performance for the gas turbine system [3].

The aim of this paper is to apply a suitable  $H_{\infty}$  controller using state space approach to reduce the effect of disturbance (torque) on the system and to achieve the design requirements.

### **2 NONLINEAR MODEL OF THE GAS TURBINE SYSTEM**

The non-linear modeling is based on the thermodynamic equations in which the behavior of the engine has been described. The major parts of a gas turbine are shown in figure.1 which include; the inlet duct, compressor, combustion chamber, turbine and nozzle or gas deflector. The interactions between these components depend on the physical structure of the engine. The air is drawn into the engine through the inlet duct by the compressor, which compresses it and then delivers it to the combustion chamber. Inside the combustion chamber the air is mixed with fuel and the mixture ignited producing a rise in temperature and hence an expansion occurs for the gases, these gases are exhausted through the engine nozzle or the engine gas-deflector. Moreover, gases pass first through the turbine which is designed to extract sufficient energy from them to keep the compressor rotating, thus the engine is self-sustaining. For gas turbine system there are three quasi polynomial differential equations as presented in equations 1, 2 and 3 respectively [4], [5].

$$\frac{dx_{1}}{dt} = x_{1} \begin{pmatrix} C_{1,1}x_{1}^{-1}x_{2}x_{3} + C_{1,2}x_{1}^{-1}x_{3} + \\ C_{1,3}x_{1}^{-1}x_{2} + C_{1,4}x_{1}^{-1} + \\ C_{1,5}x_{2}x_{3} + C_{1,6}x_{3} + \\ C_{1,7}x_{1}^{-5}x_{2}^{1.5} + C_{1,8}x_{1}^{-5}x_{2}^{5} \end{pmatrix} + b_{1}u = f_{1}(x_{1}, x_{2}, x_{3}) + b_{1}u \\
\frac{dx_{2}}{dt} = x_{2} \begin{pmatrix} C_{2} + C_{2,1}x_{3} + C_{2,2}x_{2}^{2857}x_{3} + \\ C_{2,5}x_{2}^{2857} + C_{2,6}x_{2}^{-1} + \\ C_{2,5}x_{2}^{2857} + C_{2,6}x_{2}^{-1} + \\ C_{2,9}x_{1}^{-5}x_{2}^{1.5} + C_{2,10}x_{1}^{-5}x_{2}^{5} \end{pmatrix} + b_{2}u = f_{2}(x_{1}, x_{2}, x_{3}) + b_{2}.$$

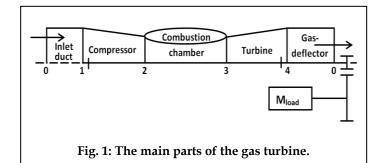
$$\frac{dx_{3}}{dt} = x_{3} \begin{pmatrix} C_{3,1}x_{2}^{2}x_{3}^{-1} + C_{3,2}x_{2}^{1.7143}x_{3}^{-1} + \\ C_{3,5}x_{1}^{-5}x_{2}^{-5}x_{3}^{-2} + C_{3,6}x_{1}^{-5}x_{2}^{22143}x_{3}^{-2} \\ + C_{3,7}x_{2}^{1.5}x_{1}^{-5}x_{3}^{-2} + C_{3,6}x_{1}^{-5}x_{2}^{22143}x_{3}^{-2} \\ + C_{3,9}x_{3}^{-2} + C_{3,10}x_{1}^{22857}x_{3}^{-1} + \\ C_{3,11}x_{3}^{-1} + C_{3,12}x_{2}^{2857}x_{3}^{-1} + \\ C_{3,15}x_{2}^{2857}x_{3}^{-2} + C_{3,14}x_{1}^{22857}x_{3}^{-2} + \\ C_{3,15}x_{2}^{2857}x_{3}^{-2} \end{pmatrix} = f_{2}(x_{1}, x_{2}, x_{3}).$$
(3)

Where

- $X_1$  is the mass in the combustion chamber  $m_{Comb}$ .
- $x_2$  is the turbine total inlet pressure  $p_3$ .
- $X_3$  is the rotational speed *n*.

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### **3** LINEARIZATION OF NONLINEAR MODEL

The general form of the state space representation of a finite dimensional non-linear time invariant (NLTI) system is [6].

$$\frac{dx(t)}{dt} = f(x(t), u(t)) \qquad (4)$$
$$y(t) = g(x(t), u(t)) \qquad (5)$$

To get Liner Time Invariant (LTI) model, it can be represented as:

$$\frac{dx(t)}{dt} = Ax^{\cdot} + Bu$$

$$y(t) = Cx + Du$$
(6)
(7)

The output of the control system (y) is rotational speed n. the disturbance is  $M_{load}$  (torque).

Let the pressure  $p_3$  is held constant

$$x_2 = x_2^0 = p_3^0 = 223587.2$$
 Pa. [3].

Let the right side of equations (1, 2, 3) denoted by f which differentiated to x1 and x2 hence, the nominal value of x is substituted in it then the constant matrices A, B, C and D that have the dimensions  $n \times n$ ,  $n \times m$ ,  $r \times n$  and  $r \times m$  respectively can be found as [4].

$$A = \partial f / dx |_{x^0, u^0}, \qquad B = \partial f / du |_{x^0, u^0}$$
$$C = \partial f / dx |_{x^0, u^0}, \qquad D = \partial f / du |_{x^0, u^0}$$

The matrices B does not depend on the state vector, which is a real constant. Then



The matrices  $C = [0 \ 1]$  and D = [0]The nominal values of x are [2, 3].

$$x^{0} = \left[ 0.00528 \text{ kg } 750 \frac{1}{\text{s}} \right]^{T}$$
  
and  $u^{0} = 0.009913$ 

By using MATLAB 7.8 program, the state space matrices A,B,C and D were found to be:

$$A = \begin{bmatrix} 0.0005 & 0.0253 \\ 0.0017 & -7.5329 \end{bmatrix}, B = \begin{bmatrix} 1 \\ 0 \\ \end{bmatrix}, C = \begin{bmatrix} 0 & 1 \\ 0 \end{bmatrix}, D = 0.$$

The nominal function of gas turbine system become as:

$$G_{nom}(s) = \frac{.0017244}{(s+7.533)(s-.0004659)}$$
(8)

The dimensionless can be used to decrees the huge difference in order between  $x_1$  and  $x_2$ .

### 4 PERFORMANCE REQUIREMENTS

The design requirements that were compatible with this paper could be summarized as follow [7].

- Good and swift disturbance rejection.
- The closed loop system is stable at all operation conditions.
- The settling time should be less than 8 seconds.
- The bandwidth of closed loop system is about (0.2-20 rad/sec).

# 5 $H_{\infty}$ Controller design and evaluation

The first step in the design procedure should start by acquiring augmented plant P(s) for the given system nominal transfer function  $G_{nom}(s)$  with the selected weighting function. The second step is to obtain iterative procedure to find the value of upper bound of the  $H_{\infty}$  norm. This would ensure the existence of sufficient conditions obtaining a stabilizing controller. The evaluation procedure included two parts. The first part is to determine the responses in the frequency domain which includes singular value plots for both open and closed loop systems to check the design requirements, the plots for the sensitivity, complementary sensitivity and control sensitivity functions. The second part is to determine the responses in the time domain which includes the plant output response. The transfer function of gas turbine system has a pole in the right side of the complex plane, this will indicate that the system is unstable. The state feedback by using pole

IJSER © 2017 http://www.ijser.org placement has utilized and then  $H_{\infty}$  controller is applied to the system. The desired selected closed loop pole is based on the required bandwidth of plant, trial and error was used to select the pole, this pole will equal [-0.08, -9]. Using MATLAB program the state feedback controller K(s) was obtained as  $K=10^3 * (0.0015, -6.3409)$  and the new transfer function of gas turbine system given as

$$G_{s}(s) = \frac{0.0017244}{(s+9)(s+0.08)}$$
(9)

### 6 $H_{\infty}$ CONTROL PROBLEM FORMULATION

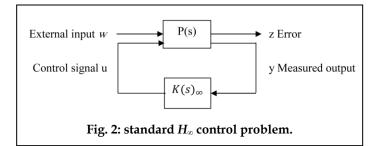
The design goals are reflected by weighting the appropriate closed-loop transfer functions in the  $H_{\infty}$  synthesis. The standard  $H_{\infty}$  control problem is shown in figure 2, and represented as

$$P(s) = \begin{bmatrix} P_{11} & P_{12} \\ P_{21} & P_{22} \\ & & \end{bmatrix}$$
(10)

The plant P(s) called augmented plant which includes the plant model and weighting function. The objective of  $H_{\infty}$  control is to calculate  $K(s)_{\infty}$  thus  $F_l(P,K)$  is minimized according to the  $H_{\infty}norm$  of the transfer function matrix  $F_l(P,K)$  that identified by the following equation [8], [9].

$$T_{zw\infty} = F_{I}(P,K)_{\infty} = max_{\omega}\overline{\sigma}(F_{I}(P,K)(j\omega)) \leq \gamma \quad (11)$$
  
Where  $\gamma \in R, \ F_{I}(P,K) =$ 
$$P_{11}(s) + P_{12}(s)k(s) \left[I - P_{22}(s)k(s)\right]^{-1}P_{21}(s)$$

The closed loop from the external w to the regular is output z and  $\sigma$  ( $F_l(P,K)(j\omega)$ ) is the largest singular value of  $F_l(P,K)$  at the frequency  $\omega$ .



It is necessary to formulate the  $H_{\infty}$  problem in terms of the sensitivity function S = (1 + GK)<sup>-1</sup>, complementary sensitivity function T = GK (1 + GK)<sup>-1</sup> and control sensitivity function R = K (1 + GK)<sup>-1</sup> [10].

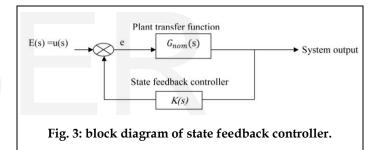
However, there is a tradeoff between these two performance criteria which can make the feedback design difficult, to assist

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in making this tradeoff, it is usual to weight the relevant sensitivity function S(s) therefore the design is able to emphasize the appropriate properties at the different frequencies. The most common approach is to keep  $|\mathbf{S}(\mathbf{j}\omega)|$  small at low frequencies, and keep  $|\mathbf{T}(\mathbf{j}\omega)|$  small at high frequencies. Now for the gas turbine system  $F_l(P,K)$  is chosen to be a function of S, T and R. The weights are the major design parameters in any  $H_{\infty}$  design. The following guidelines summarize how to choose the weights [11].

- 1. Choose the transfer function (filter) W<sub>p</sub>(s) as a low frequency weight to insure good tracking and output disturbance rejection.
- 2. Choose W<sub>u</sub>(s) as a weight on the actuator inputs to prevent actuator saturation and achieve robustness to plant additive perturbations.
- 3. Choose W<sub>o</sub>(s) as a high frequency weight to limit the closed loop bandwidth, ensure robustness to plant output multiplicative perturbations.
- 4. Keep the degree of the weights as low as possible because the degree of the controller generally equals the degree of the plant plus the degree of the weights.

To construct the augmented system as shown in figure 3, let z be the regulated output vector, w be the external input vector, x the state vector of the augmented system.



There are four conditions for stability and performance can be derived as follows:

- i. Nominal stability (NS): for figure 4 assuming ( $\Delta$ =0), all poles of the closed loop  $T_{zw}$  must be lie in left half complex plane to satisfy the nominal stability.
- ii. Robust stability (RS): condition for robust stability is

$$RS \Leftrightarrow |T| < |1/W_o|, \forall \omega$$

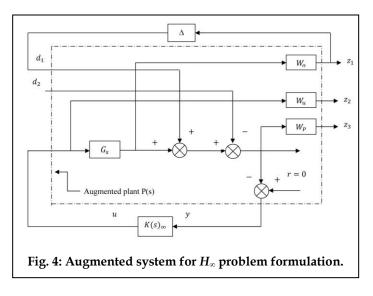
iii. Nominal performance (NP): To obtain the nominal performance assume  $\Delta$ =0 then condition for nominal performance becomes

$$NP \Leftrightarrow |S| < |1/W_p|, \forall \omega$$

iv. Robust performance (RP): the condition for robust performance is

$$RP \Leftrightarrow max_{\omega} \left( \left| W_{P} S \right| + \left| W_{O} T \right| \right) < 1$$

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### 7 SIMULATION RESULTS AND DISCUSSION

The weighting functions are chosen by trial and error. The following set weighting function is chosen to reflect the desired performance

 $W_{p} = \frac{0.4 \, s + 0.22}{s + 0.0003}$  (Good tracking and output disturbance rejection)

 $W_u = 10^{-4}$  (Prevent saturation & introduce robustness to additive uncertainties)

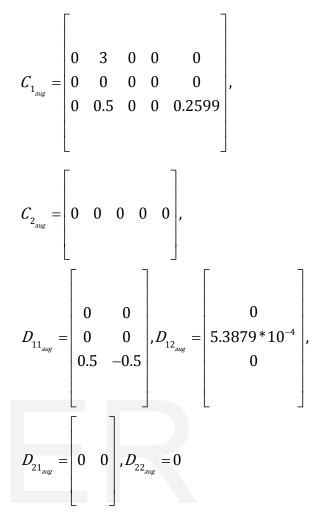
The Uncertainty weighting filter was chosen to be in the following form:

 $W_o = \frac{3s + 20.81}{s + 24.19}$  (To limit the closed loop bandwidth &

introduce robustness to plant output multiplicative uncertainties)

The state space representations are found to be:

$$A_{aug} = \begin{bmatrix} -0.6 & 2.0135 * 10^{3} & 0 & 0 & 0 \\ 0.001 & -7.5329 & 0 & 0 & 0 \\ 0 & 8 & 0 & 0 & 0 \\ 0 & 0 & 0 & -24.1935 & 0 \\ 0.5 & 0 & 0 & 0 & -3*10^{-4} \end{bmatrix}$$
$$B_{1_{aug}} = \begin{bmatrix} 0 & 0 \\ 0 & 0 \\ 0 & 0 \\ 0 & 0 \\ 0.5 & -0.5 \end{bmatrix}, B_{2_{aug}} = \begin{bmatrix} 1 \\ 0 \\ 0 \\ 0 \\ 0 \\ 0 \end{bmatrix}$$



- A Value of *γ<sub>min</sub>* of the optimal solution equals to 1.2482 and the *H<sub>∞</sub>* norm of the closed loop transfer function *||T<sub>zw</sub>(S)||*<sub>∞</sub> equals to 1.2482 this means that the controller is admissible.
- The *H*<sub>∞</sub> robust controller is suboptimal with transfer function given as:

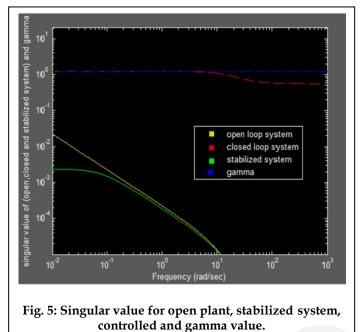
$$k(s)_{\infty} = \frac{121868.7452(s+0.08)(s+9)(s+24.19)}{(s+24.1)(s+0.0003)(s^{2}+26.45s+187)}$$

 The pole of closed loop are found to be: -0.0003, -24.1935, -0.0800, -1.3863, -9, -10.3345, -14.7327, -24.0937

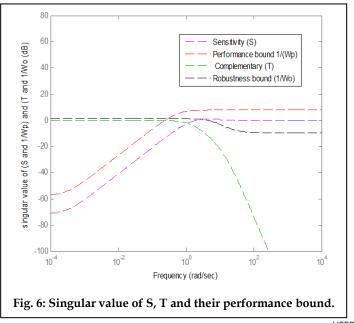
All the poles of closed loop system lie in the left side of the complex plane, so the nominal stability is guaranteed.

• The singular value of open loop plant, stabilized plant system and state feedback  $H_{\infty}$  controlled systems are all shown in figure 5. The maximum singular value of three loop systems that obtained are (0.4804 db,

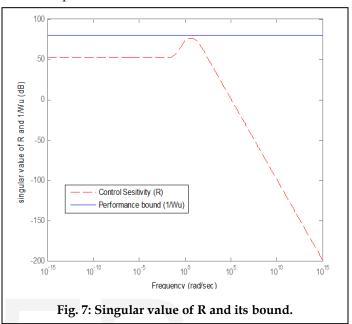
IJSER © 2017 http://www.ijser.org 0.0024 db, 1.24 db) respectively. As it can be seen, the closed loop of state feedback  $H_{\infty}$  controlled system is stable over required range until the rolling will be start at (10 rad/sec).



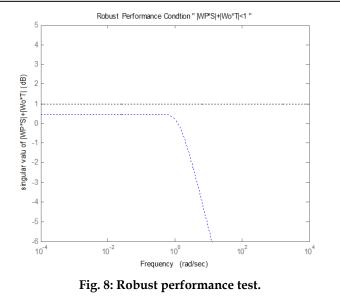
- The conditions for nominal performance NP, robust stability RS and robust performance RP can be summarized as follows:
- Nominal performance NP: In figure 6, the singular value of sensitivity function S which gained is (1.03 db at 6.12 rad/sec) and  $|W_P|$  equals (7.92 db at 2.15 rad/sec). In this figure, a good coverage for sensitivity function by its bound can be shown. At the same time, the sensitivity function keeps a smooth shape without resonant peak.



• In figure 7, the singular value for the control sensitivity function R that found is (76.8 db at 9.12 rad/sec) and performance bound  $|W_u|$  equals (80 db at 4.24 rad/sec), it can be seen in this figure that control sensitivity function is totally surrounded by its performance bound.



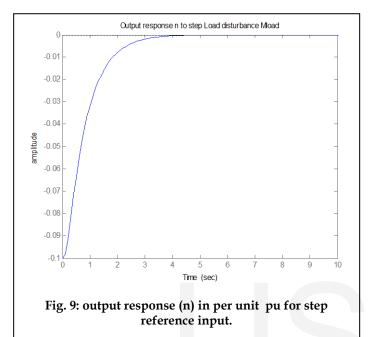
• Robust stability RS: In figure 6, the singular value of complementary sensitivity function T that obtained is (-0.336 db at .429 rad/sec) and  $|W_o|$  equals (1.92 db at .429). A very sharp roll off to the complementary sensitivity function is achieved by the  $H_{\infty}$  controller, this is an indication that the high frequency of any uncertainty or noise is being attenuated. It can be seen that the system has been yield to the condition  $max|W_P S| + |W_o T| < 1$  and the nominal performance becomes satisfied as shown in figure 8.

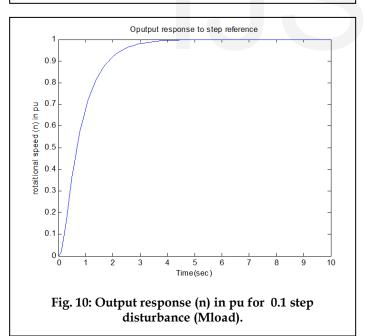


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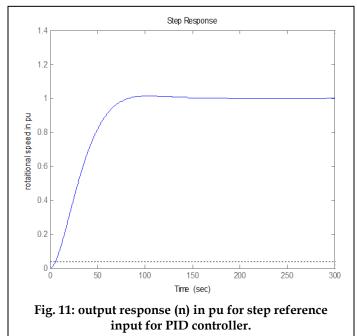
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• The time domains results were illustrated in figure 9 and 10. In figure 9, the system responses to step input which was applied at the reference r. whereas in figure 10 the system responses to 0.1 step inputs, this figure offered a good rejection for disturbance with settling time of (5 sec) and the response has no overshoot.





• Figure 11 illustrates the output response for PID controller. The comparison between the figures 10 and 11 shows that the output response for  $H_{\infty}$  controller is best and has salting time less than PID controller.



### 8 CONCLUSION

In this paper the new  $H_{\infty}$  controller is presented based on state space approach using MATLAB environment. The state feedback (pole placement) approach has been employed to stabilize the system by applying  $H_{\infty}$  controller. It has been shown that  $H_{\infty}$  controller gives faster response than the PID controller in addition to obtain a robust control system. Less settling time has been investigated by picking appropriate weighting function, it has been done by the method of try and error. For choosing suitable weighting filters, design experience and knowledge of the plants are the most assistant factors.

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